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(54) Title: METHOD FOR PRODUCING A SUSPENSION OF HYDROXYLAPATITE			
(57) Abstract			
<p>The invention is concerned with an improved hydroxylapatite HAP composition in the form of a suspension or paste. The improvement is that the composition may have a homogeneous concentration in the range of from 7 % to 96 %. The invention is also concerned with a method for producing the homogeneous concentration compositions of HAP and their industrial applications.</p> <p><i>no mention of surface active agents ~ protective colloids</i></p> <p><i>anisometric bar like shape page 4 lines 27-28 page 6 lines 19:20 claims 1 and 9</i></p>			

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## METHOD FOR PRODUCING A SUSPENSION OF HYDROXYLAPATITE

Field of the invention

The present invention is concerned with a hydroxylapatite composition having a homogeneous concentration within the range of from 7 % to 96 %. The present invention also relates to a method for preparing the hydroxylapatite compositions and products containing the hydroxylapatite compositions and its use in specific applications.

Hydroxylapatite (HAP) may be used in medicine as a denture material, prophylactic additive in tooth pastes and medicinal solutions, chewing gums, sorbents for medicinal preparations and various organic and inorganic compounds, in materials for stamatology and bone surgery and as a filler or sorbent agent for gas-liquid chromatography.

State of the Art

Due to the fields of application of hydroxylapatite the availability of pure HAP, free from other calcium phosphates has become the main requirement. Furthermore, it became highly desirable to prepare HAP not only in powder form but as a suspension or paste of a predetermined composition.

A known method for producing hydroxylapatite is based on the mixing of a suspension of calcium hydroxyde with an aqueous solution of phosphoric acid, wherein either the reaction product of both components or the mixture is treated by a grinding operation that ensures a mechano-chemical activation of the reagents. According to this method as a grinding apparatus there may be used mills and crushers of various types and as a

grinding medium glass beads, aluminium balls and the like. According to this method hydroxylapatite having large crystals is mainly produced.

This method does not allow to produce fairly pure hydroxylapatite and moreover the preparation of suspensions and pastes from hydroxylapatite having large crystals is practically impossible (Patent of Japan No. 62-43524, 1987).

Furthermore, a method for producing hydroxylapatite is known from the Russian Federation patent application no.

93012609/26, filed on March 9, 1993 which is forming the technical background of the present invention. According to this method a suspension of calcium hydroxide is reacted with phosphoric acid in a closed multiple circuit whereby the suspension of calcium hydroxide is past through two zones. In the first zone a continuous supply of phosphoric acid in the amount necessary to reach pH=10-11 is provided. The suspension flow rate in the first zone is 0.8 m/s to 1.5 m/s and the residence time is 1.0 s to 1.5 s. In the second zone the obtained mixture is diluted by 400 to 500 times with a suspension of calcium hydroxide. The diluted mixture is returned to the first zone and the process is repeated thereby ensuring a 4 to 5 fold circulation of the complete volume of the mixture during 10 to 20 min. After the feeding of acid is terminated the obtained suspension of the product is stirred for additionally 10 to 12 min. The resulting suspension of hydroxylapatite has a concentration of 4.5 % to 5.0 %. Additionally, the suspension may be dried to produce solid hydroxylapatite or dehydrated by centrifugation to produce a suspension of hydroxylapatite having a concentration of 18 % to 33 %.

This method ensures the production of a pure product with a desired composition and the yield is 99.5 % to 99.8 % of the theoretical one and increases the technological adaptability of the process.

A disadvantage of this known method, however, is that a suspension with homogeneous concentration can not be obtained.

The preparation of highly concentrated suspensions of more than 18 % is time-consuming, requires large volumes of apparatus and the production of a suspension with a concentration higher than 33 % is practically impossible.

#### Description of the invention

The present invention is based on the problem to produce a suspension of hydroxylapatite with any necessary concentration, i.e. either less than 18 % or more than 33 % and as well pastes of hydroxylapatite having a homogeneous concentration composition.

According to the present invention a hydroxylapatite (HAP) composition is provided, wherein the dimensions of the hydroxylapatite particles is 0.01  $\mu\text{m}$  to 0.02  $\mu\text{m}$  in width and 0.5  $\mu\text{m}$  to 0.1  $\mu\text{m}$  length, the composition having a homogeneous concentration within the range of from 7 % to 96 %. 500-100 nm

Preferred concentration ranges are given in subclaims 2 to 6. The composition may be in the form of a suspension or paste.

The hydroxylapatite (HAP) compositions of this invention are starting from a suspension of hydroxylapatite with a concentration of 4.5 % to 5.0 % which may be obtained preferably according to the method of the patent of the Russian Federation mentioned above. According to the invention such a suspension is subjected to alternating stirring and filtration ranges with the stirring being carried out at a rate of 0.8 m/s to 3.0 m/s for 5 to 25 minutes and each stage is providing increasing homogeneous concentrations of hydroxylapatite due to increased stirring rates and/or times. Thus, suspensions with concentrations of 7 % to 20 % in a first step, 21 % to 34 % in a second step, 35 % to 45 % in a third step, 46 % to 62 % in a fourth step, 63 % to 75 % in a fifth step can be obtained. The yield of the final pro-

duct is made from any step, as far as the necessary concentration is reached.

The method is based on the mechano-structural thixotropic properties of a dispersed system of hydroxylapatite which method consists in effecting reversible sol-gel transitions usually occurring upon mechanical stress by compulsory means.

It is noteworthy that the change of the structural mechanical, i.e. the thixotropic properties of disperse systems depend on the size and form of the particles forming this system. In rough disperse systems (particle sizes of 1  $\mu\text{m}$  and more) the number of coagulation contacts is not sufficient to produce a sol and to effect the sol-gel transitions by means of mechanical stress. Therefore, the mechanical treatment of suspensions with particle sizes of 1  $\mu\text{m}$  and more practically does not result in the change of its rheological properties.

The dimensions of the particles used in the synthesis of hydroxylapatite HAP are 0.01  $\mu\text{m}$  to 0.02  $\mu\text{m}$  in width and 0.05  $\mu\text{m}$  to 0.1  $\mu\text{m}$  in length permitting to utilize the thixotropic properties of the produced HAP suspension and to develop a method to specifically concentrate such suspensions. The mentioned dimensions and shapes of particles of the initial hydroxylapatite favour the formation of coagulation structures due to cohesion of the particles by Van der Waals forces interacting with links, chains, spatial nets, frameworks of the primary particles, their chains and aggregates. The centers of the point contacts appear at the ends of particles. Therefore, an anisometric, especially bar-like shape of the particles is favourable to form such structures. The afore-mentioned ratio between width and length of the particles of the initial HAP satisfies this requirement. Such systems are able to undergo reversible sol-gel transitions, i.e. to repeatedly form and destroy their structure.

Thus, it was found that during a stirring of the suspension having a concentration of 4.0 % to 5.0 % depending on the inten-

sity and duration of stirring a partial or complete destruction of its structure occurs along with the transition of the sole into a gel. A subsequent filtration of the hydrogel results in a partial separation of the solvent (water) thereby concentrating the disperse system up to 7 % to 20 % and in the transition of the gel into a sol which has a spatial structure and stability formed at the expense of cohesion and aggregation of particles of the disperse phase, preventing its further filtration and concentration.

During further stirring the formed stable spatial structure depending on the intensity and duration of stirring is again partially or completely destroyed with the formation of a gel. The subsequent filtration of the hydrogel results in a partial and controlled separation of water, in concentrating the disperse system up to a concentration of 21 % to 34 % and the transition of the gel into a spatially structured and stable sol that practically prevents its further filtration and concentration. The same process occurs in all the subsequent stages of concentrating the suspension. The number of stages varies depending on the necessity to produce a suspension of a predetermined and required concentration.

From the above it can be seen, that the concentration of a suspension is a determining fact at each stage of the process. To adjust a desired concentration it is necessary to set specific conditions at the stage of stirring, e.g. rate and time, that in turn will depend on the type of the apparatus used, e.g. a tank with agitator, vibratory mill, vibrators with variable repetition and amplitude and so on and its volume. These parameters are selected in each case to produce a suspension of the desired concentration.

The method is illustrated by the following example(s).

Example 1

554.6 g of anhydrous calcium oxide are introduced into a reactor

containing distilled water at ambient temperature and distilled water is added until a solid/liquid ratio of S:L = 1:35 is obtained. In a separate tank calcium hydroxide and the phosphoric acid in an amount that it is necessary to reach a pH of 10 are added. The residence time of the mixture in this tank is 1.0 s (the first zone).

Afterwards the mixture of the reaction products is supplied into the second tank (the second zone of reaction) where they are diluted with a suspension of calcium hydroxide by 400 times. The complete volume of the mixture containing calcium hydroxide and hydroxylapatite is circulated in a closed circuit combining the first and second zone. The circulating factor is 4. After this the phosphoric acid supply into the first zone is terminated and the suspension is stirred for 10 min.

As a result the pure stoichiometric hydroxylapatite in a suspension form is produced free of admixtures and having a hydroxylapatite concentration of 4.0 % to 5.0 %. The Ca/P ratio is 1.67 in the produced sample. The specific surface area is 100 m<sup>2</sup>/g. The dimensions of the HAP crystals are 0.01 μm to 0.02 μm in width and 0.05 μm to 0.1 μm in length.

The produced suspension then is stirred for 7 min with the suspension flow rate equal to 0.8 m/s. Upon filtration a suspension (paste) with a concentration of 14.8 % is prepared. Afterwards this suspension is stirred for 10 min with a suspension flow rate of 1.2 m/s and filtrated until a suspension (paste) with concentration of 26.6 % is obtained. Then this suspension is again liquefied by means of agitation for 10 min at a suspension flow rate of 2 m/s and filtrated to produce a suspension (paste) with a concentration of 39.9 %. The produced paste shows a homogeneous composition and homogeneous properties.

The conditions for producing suspensions of different concentrations may be illustrated by the following Table, where t is the time of treatment of the suspension in min, v is the stirring rate in m/s, C is the concentration of the HAP suspension

based on the solid phase content in %, No. is the sample number and YP is the yield of the final product at the specified stage of the suspension processing.

The range of the agitation rate is determined by the aggregation degree of a suspension and by its concentration. At agitating rates lower than 0,8 m/s the sol destruction practically does not occur, even for suspensions of an initial concentration of 4 % to 5 % of HAP. At rates above 3.0 m/s the capturing of air bubbles and aeration of the suspension deteriorating of the product quality occurs requiring additional operations to expel them.

The present invention allows to provide suspensions (pastes) of hydroxylapatite having a composition that is determined by the field of their application. Suspensions (pastes) of hydroxylapatite possess an improved quality. A selection of the product at any stage allows to produce suspensions or pastes in a wide range of concentrations from 7 % to 96 %, the produced pastes having a homogeneous composition that provides substantially easy conditions for their application and handling.

Claims

1. A hydroxylapatite (HAP) composition wherein the dimensions of the hydroxylapatite particles are 0,01  $\mu\text{m}$  to 0,02  $\mu\text{m}$  in width and 0,5  $\mu\text{m}$  to 0,1  $\mu\text{m}$  in length, the composition having a homogeneous concentration within the range of from 7 % to 96 %.
2. The composition of claim 1, having a homogeneous concentration of HAP between 7 % to 20 %.
3. The composition of claim 1, having a homogeneous concentration of HAP between 21 % to 34 %.
4. The composition of claim 1, having a homogeneous concentration of HAP between 35 % to 45 %.
5. The composition of claim 1, having a homogeneous concentration of HAP between 46 % to 62 %.
6. The composition of claim 1, having a homogeneous concentration of HAP between 63 % to 75 %.
7. The composition of claims 1 to 6 being in the form of a suspension.
8. The composition of claims 1 to 6 being in the form of a paste.
9. A method for preparing hydroxylapatite compositions with predetermined homogeneous concentration ranges between 7 % to 96 %, wherein as a starting material a 4 % to 5 % aqueous composition of hydroxylapatite (HAP) having particle dimensions of 0,01  $\mu\text{m}$  to 0,02  $\mu\text{m}$  in width and 0,05 to 0,1  $\mu\text{m}$  in lenght is

subjected to alternating stirring and filtration stages with the stirring being carried out at a rate of from 0,8 m/s to 3,0 m/s for 5 min to 25 min, each stage thereby providing increasing homogeneous concentrations of HAP due to increasing stirring rates and/or times.

10. A denture material containing as a component a hydroxylapatite composition of claims 1 to 8 or obtained by the method of claim 9.

11. A tooth paste containing as a component a hydroxylapatite composition of claims 1 to 8 or obtained by the method of claim 9.

12. A chewing gum containing as a component a hydroxylapatite composition of claims 1 to 8 or obtained by the method of claim 9.

13. A sorbent material for gas-liquid chromatography consisting of a hydroxylapatite composition of claims 1 to 8 or obtained by the method of claim 9.

14. Use of a composition of claims 1 to 8 or obtained by the method of claim 9 for providing a preparation to be used in the field of stomatology.

15. Use of a composition of claims 1 to 8 or obtained by the method of claim 9 for providing a preparation to be used in bone surgery.

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TABLE

No.	PROCESSING STAGES										IV			V		
	I			II			III			IV			V			
	t	v	C	t	v	C	t	v	C	t	v	C	t	v	C	
1.	7	0.9	16.3													
2.	5	0.8	12.5	8	1.2	22.3										
3.	10	1.0	17.9	12	1.3	31.3	12	1.9	42.1							
4.	10	1.2	19.2	12	1.5	34.1	15	2.0	44.2	15	2.5	56.1				
5.	7	0.8	14.8	10	1.2	26.6	10	2.0	39.9	15	2.5	56.6	25	3	75	
													YP			

**INTERNATIONAL SEARCH REPORT**

International Application No  
PCT/IB 97/01414

<b>A. CLASSIFICATION OF SUBJECT MATTER</b>				
IPC 6	C01B25/32	B01J20/04	G01N30/48	A61K6/033
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**B. FIELDS SEARCHED**

Minimum documentation searched (classification system followed by classification symbols)  
IPC 6 C01B B01J G01N

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

**C. DOCUMENTS CONSIDERED TO BE RELEVANT**

Category	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	EP 0 664 133 A (AKTSIONERNOE OBSCHESTVO ZAKRYT) 26 July 1995 see the whole document ---	1-4, 14, 15
X	EP 0 261 458 A (TOA NENRYO KOGYO KK) 30 March 1988 see the whole document ---	1-5, 13
A	EP 0 486 813 A (BENCKISER KNAPSACK LADENBURG) 27 May 1992 see the whole document ---	1, 9, 11, 12, 15
A	US 3 873 327 A (DUFF EDWARD JOHN) 25 March 1975 see the whole document ---	10 -/-

Further documents are listed in the continuation of box C.

Patent family members are listed in annex.

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## C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT

Category	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	US 5 468 489 A (SAKUMA SHUJI ET AL) 21 November 1995 see the whole document ---	11
A	WO 94 20416 A (AKTSIONERNOE OBSCHESTVO ZAKRYT ; KOMAROV VLADIMIR F (RU); MELIKHOV) 15 September 1994 cited in the application ----	

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